Amendment to the Claims:

This listing of claims will replace all prior versions of claims in the application:

- (Currently amended) In a method of making a sheet from a fibrous furnish, the
 improvement which comprises preparing a nascent web while controlling its porosity and
 at least partially throughdrying said web wherein airflow through said sheet exhibits a
 characteristic Reynolds Number based on flow parameters in the sheet of less than about
 1 and a characteristic dimensionless throughdrying coefficient based on flow parameters
 in the sheet of from about 4 to about 10.
- 2. (Original) The improvement according to claim 1, wherein the airflow through said sheet exhibits by a characteristic Reynolds Number of less than about 0.75.
- (Original) The improvement according to Claim 2, wherein the airflow through said sheet exhibits a characteristic Reynolds Number of less than about 0.5.
- 4. (Original) The improvement according to Claim 1, wherein airflow through said sheet exhibits a characteristic Reynolds Number of less than about 0.75 and a characteristic dimensionless throughdrying coefficient of from about 5 to about 7.
- 5. (Original) The improvement according to Claim 1, wherein said sheet is an absorbent sheet prepared from a cellulosic furnish and characterized by a hydraulic diameter of from about 3 x 10⁻⁶ ft to about 8 x 10⁻⁵ ft with the provisos: (a) that when the void volume fraction of said sheet exceeds about 0.72, the hydraulic diameter of the sheet is less than about 8 x 10⁻⁶ ft; and (b) that when the void volume fraction of the sheet exceeds about 0.8, said hydraulic diameter of said sheet is less than about 7 x 10⁻⁶ ft and wherein further said absorbent sheet is characterized by a wet springback ratio of at least about 0.6.
- (Originat) The improvement according to Claim 5, wherein said absorbent sheet is characterized by a wet springback ratio of at least about 0.65.

- 7. (Original) The improvement according to Claim 6, wherein said absorbent sheet is characterized by a wet springback ratio of between about 0.65 and about 0.75.
- (Original) The improvement according to Claim 7, wherein said absorbent sheet is characterized by a hydraulic diameter of from about 4 x 10⁻⁶ ft to about 6 x 10⁻⁵ ft.
- (Original). The improvement according to Claim 5, wherein said absorbent sheet is characterized by a hydraulic diameter of between about 4 x 10⁻⁶ ft and about 8 x 10⁻⁶ ft.
- 10. (Original) The improvement according to Claim 8, wherein said absorbent sheet is characterized by a hydraulic diameter of up to about 7×10^{-6} ft.
- 11. (Original) The improvement according to Claim 1, wherein said sheet is prepared from a fibrous furnish comprising fiber other than virgin cellulosic fiber.
- 12. (Original) The improvement according to Claim 11, wherein said furnish comprises a non-wood fiber selected from the group consisting of straw fibers, sugarcane fibers, bagasse fibers and synthetic fibers.
- (Original) The improvement according to Claim 11, wherein said absorbent sheet comprises recycled fiber.
- 14. (Original) The improvement according to Claim 13, wherein the recycled fiber in said absorbent sheet comprises at least about 50 percent by weight of the fiber present in the sheet.
- 15. (Original) The improvement according to Claim 14, wherein the recycled fiber present in said absorbent sheet comprises at least about 75 percent by weight of the fiber present in the sheet.
- 16. (Original) A wet crepe, throughdry process for making sheet comprising the steps of:

- (a) depositing an aqueous fibrous furnish on a foraminous support;
- (b) compactively dewatering said furnish to form a web;
- (c) applying said dewatered web to a heated rotating cylinder and drying said web to a consistency of greater than about 30 percent and less than about 90 percent; and
- (d) creping said web from said heated cylinder at said consistency of greater than about 30 percent and less than about 90 percent;
- (e) throughdrying said web subsequent to creping said web from said heated cylinder to form said sheet.

wherein the furnish composition and processing of steps (a), (b) and(c), as well as the creping geometry, temperature profile of the web upon creping, moisture profile of the web upon creping, and web adherence to the heated rotated cylinder are controlled such that airflow through said sheet exhibits a characteristic Reynolds Number of less than about 1 and a characteristic dimensionless throughdrying coefficient of from about 4 to about 10.

- 17. (Original) The process according to Claim 16, wherein said sheet has a basis weight of at least about 12 lbs per 3,000 ft².
- (Original) The process according to Claim 17, wherein said sheet has a basis weight of at least about 15 lbs/3000 ft².
- 19. (<u>Original</u>) The process according to Claim 18, wherein said sheet has a basis weight of at least about 20 lbs/3000 ft².
- 20. (Original) The process according to Claim 19, wherein said sheet has a basis weight of at least about 25 lbs/3000 ft².
- (Original) The process according to Claim 20, wherein said sheet has a basis weight of at least about 30 lbs/3000 ft².

- 22. (Original) The process according to Claim 16, wherein said web is dewatered to a consistency of at least about 30 percent prior to being dried on said heated cylinder.
- (Original) The process according to Claim 22, wherein said web is dewatered to a
 consistency of at least about 40 percent prior to being dried on said heated cylinder.
- 24. (<u>Original</u>) The process according to Claim 23, wherein said web is dried to a consistency of at least about 50 percent on said heated cylinder prior to being creped.
- 25. (Original) The process according to Claim 16, wherein said web is dried to a consistency of at least about 60 percent on said heated cylinder prior to being creped.
- 26. (Original) The process according to Claim 25, wherein said web is dried to a consistency of at least about 70 percent on said heated cylinder prior to being creped.
- 27. (Original) The process according to Claim 16, wherein said web is creped from said heated cylinder utilizing a creping blade and a creping angle of from about 50 to about 125 degrees.
- 28. (Original) The process according to Claim 16, wherein said web is creped from said heated cylinder in a creping rip utilizing a creping fabric traveling at a speed slower than the speed of said heated rotating cylinder.
- 29. (Original) The process according to Claim 16, wherein said web is creped from said heated cylinder with an undulatory creping blade so as to form a reticulated biaxially undulatory product with crepe bars extending in the cross direction and ridges extending in the machine direction.
- 30. (Original) The process according to Claim 29, wherein said undulatory creping blade is positioned, configured and dimensioned so as to be in continuous undulatory engagement with said heated rotating cylinder over its width.

- 31. (Original) The process according to Claim 30, wherein said product comprises from about 8 to about 150 crepe bars per inch.
- 32. (Original) The process according to Claim 29, wherein said product comprises from about 4 to about 50 ridges per inch extending in the machine direction.
- 33. (Original) The process according to Claim 16, wherein said sheet is prepared from a fibrous furnish comprising fiber other than virgin cellulosic fiber.
- 34. (Original) The process according to Claim 33, wherein said furnish comprises a nonwood fiber selected from the group consisting of straw fibers, sugarcane fibers, bagasse fibers and synthetic fibers.
- 35. (Original) The process according to Claim 16, wherein said aqueous furnish comprises recycled fiber.
- 36. (Original) The process according to Claim 35, wherein the recycled fiber in said aqueous furnish comprises at least about 50 percent by weight of the fiber present.
- 37. (Original) The process according to Claim 36, wherein the recycled fiber present in said aqueous furnish comprises at least about 75 percent by weight of the fiber present.
- 38. (Original) The process according to Claim 37, wherein the cellulosic fiber present in said aqueous furnish consists essentially of recycled fiber.
- 39. (Original) The process according to Claim 16, wherein said step of compactively dewatering said web comprises wet-pressing said web in a transfer nip including a press roll and said heated rotating cylinder.
- 40. (Original) The process according to Claim 16, wherein said step of compactively dewatering said web comprises wet-pressing said web in a controlled pressure shoe press.

- (Original) The process according to Claim 40, wherein said web is disposed on a
 papermaking felt in said controlled pressure shoc press.
- 42. (Original) The process according to Claim 16, wherein said step of compactively dewatering said furnish comprises pressing said furnish in a press nip providing a peak engagement pressure of from about 500 to about 2000 kN/m².
- 43. (Original) The process according to Claim 42, wherein said press nip is provided with an overall line load of less than about 90 kN/m.
- 44. (Original) The process according to Claim 16, wherein said step of compactively dewatering said furnish comprises pressing said furnish in a press nip providing a peak engagement pressure of at least about 2,000 kN/m² at an overall line load of less than about 240 kN/m.
- 45. (Original) The process according to Claim 44, wherein said press nip imposes an asymmetric pressure distribution on the furnish, said pressure distribution being skewed such that the pressure declines from a peak pressure to a value of 20% of said peak pressure over a nip length which is no more than about half of the nip length over which it rose to said peak pressure from 20% of said peak pressure.
- 46. (Original) The process according to Claim 44, wherein said line load is less than about 175 kN/m.
- 47. (Original) The process according to Claim 46, wherein said line load is less than about 90 kN/m.
- 48. (Original) The process according to Claim 44, wherein the peak engagement pressure in said press nip is at least about 2,500 kN/m².
- 49. (<u>Original</u>) The process according to Claim 48, wherein the peak engagement pressure in said press nip is at least about 3,000 kN/m².

- 50. (Original) The process according to Claim 16, wherein said aqueous furnish comprises a chemical additive.
- 51. (Original) The process according to Claim 50, wherein said chemical additive comprises surface modifiers, softeners, debonders, strength aids, latexes, opacifiers, optical brighteners, dyes, pigments, sizing agents, barrier chemicals, retention aids, insolubilizers, organic or inorganic crosslinkers, and combinations thereof; said chemicals optionally comprising polyols, starches, PPG esters, PEG esters, phospholipids, surfactants, polyamines and the like.
- (Original) The process according to Claim 51, wherein said aqueous furnish comprises a cationic debonding agent.
- 53. (Original) The process according to Claim 52, wherein said aqueous furnish further comprises a nonionic surfactant.
- 54. (Original) The process according to Claim 16, further comprising transferring said creped web over an open draw at a speed of at least about 2000 fpm while aerodynamically supporting said web to preserve the creped structure thereof.
- 55. (Original) The process according to Claim 54, further comprising transferring said creped web over an open draw at a speed of at least about 2500 fpm while aerodynamically supporting said web to preserve the creped structure thereof.
- 56. (Original) The process according to Claim 55, wherein said web is transferred over said open draw at a speed of at least about 3000 fpm.
- 57. (Original) The process according to Claim 56, wherein said web is transferred over said open draw at a speed of at least about 4000 fpm.

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- 58. (Original) The process according to Claim 57, wherein said web is transferred over said open draw at a speed of at least about 5000 fpm.
- 59. (Original) The improvement according to Claim 16, wherein subsequent to creping from said heated rotating cylinder, said web is throughair dried at a rate of at least about 30 pounds of water removed per square foot of throughair drying surface per hour.
- 60. (Original) The improvement according to Claim 59, wherein said web is throughair dried at a rate of at least 40 pounds of water removed per square foot of throughair drying surface per hour.
- 61. (Original) The improvement according to Claim 60, wherein said web is dried by throughair drying at a drying rate of at least about 50 pounds of water removed per square foot of throughair drying surface per hour.
- 62. (Original) The method according to Claim 16, wherein said step of depositing said aqueous furnish on said foraminous support includes foam-forming said furnish on said foraminous support.
- 63. (Original) The method according to Claim 62, wherein said furnish is a foamed furnish and comprises from about 150 to about 500 ppm by weight of a foam-forming surfactant.
- 64. (<u>Original</u>) The method according to Claim 62, wherein said foamed furnish has a consistency of from about 0.1 to about 3 percent.
- 65. (<u>Original</u>) The method according to Claim 16, wherein at least about 5 percent of the fiber in said aqueous furnish has been subjected to a curling process.
- 66. (Original) The method according to Claim 65, wherein at least about 10 percent of the fiber in said aqueous furnish has been subjected to a curling process.

- 67. (Original) The method according to Claim 66, wherein at least about 25 percent of the fiber in said aqueous furnish has been subjected to a curling process.
- 68. (Original) The method according to Claim 67, wherein at least about 50 percent of the fiber in said aqueous furnish has been subjected to a curling process.
- 69. (Original) The method according to Claim 68, wherein at least about 75 percent of the fiber in said aqueous furnish has been subjected to a curling process.
- 70. (Original) The method according to Claim 69, wherein at least about 90 percent of the fiber in said aqueous furnish has been subjected to a curling process.
- 71. (Original) The method according to Claim 65, wherein said method of curling said fiber comprises concurrently heat-treating and convolving said fiber at an elevated temperature.
- 72. (Original) The method according to Claim 71, wherein said fiber is curled in a disk refiner with saturated steam at a pressure of from about 5 to about 150 psig.
- 73. (Original) The method according to Claim 16, further comprising the step of pressure molding said web subsequent to creping said web by deflecting said web into an impression fabric.
- 74. (Original) The method according to Claim 16, wherein said dewatered web is dried to a consistency of greater than about 60 percent on said heated rotating cylinder prior to being creped therefrom and re-wet with an aqueous composition subsequent to being creped from said heated rotating cylinder.

- 75. (Original) The method according to Claim 74, wherein said aqueous composition includes a process additive or functional additive.
- 76. (Original) The method according to Claim 75, wherein said additive comprises a softener, a debonder, starch, strength aids, retention aids, barrier chemicals, wax emulsions, surface modifiers, antimicrobials, botanicals, latexes, binders, absorbency aids, and combinations thereof, said additives optionally including phospholipids, polyamines, PPG esters, PEG esters and polyols.
- 77. (Original) The method according to Claim 76, wherein said additive is selected from the group consisting of wet strength resins, dry strength resins and softeners.
- 78. (Original) The method according to Claim 74, wherein said web is re-wet to a consistency of less than about 60 percent and subsequently wet-molded on an impression fabric.
- 79. (Original) A method of making absorbent sheet from an aqueous cellulosic furnish comprising:
 - (a) depositing said aqueous furnish on a foraminous support to form a nascent web;
 - (b) compactively dewatering said web in a transfer nip while transferring said web to a Yankee cylinder;
 - (c) drying said web to a consistency of from about 30 to about 90 percent on said Yankee cylinder;
 - (d) creping said web from said Yankee cylinder;
 - (e) transferring said web over an open draw to a throughdrying fabric while aerodynamically supporting said web;
 - (f) re-wetting said web with an aqueous composition;
 - (g) wet molding said re-wet web on said throughdrying fabric; and
 - (h) throughdrying said re-wet web wherein airflow through said sheet exhibits a characteristic Reynolds Number of less than about 1 and a characteristic dimensionless throughdrying coefficient of from about 4 to about 10.

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Claims 80-205 (Canceled, as drawn to non-elected inventions.)